## <u>AMENDMENTS TO THE CLAIMS</u>

## IN THE CLAIMS:

- 1. (Currently Amended) An elimination process of fluorinated anionic <u>surfactants</u> sufactants from exhausted gaseous streams wherein the gaseous stream is put into contact with aqueous solutions having pH from 3.5 to 13.8, the aqueous solution density being lower than 1.05 g/cm<sup>3</sup>, preferably lower than 1.03 g/cm<sup>3</sup>, wherein the concentration in the aqueous solution of the fluorinated anionic surfactant removed from the gaseous stream is lower than or equal to 70 ppm, preferably lower than or equal to 60 ppm, still more preferably lower than 50 ppm.
- (Currently Amended) A <u>The</u> process according to claim 1, wherein the anionic fluorinated surfactants are selected from perfluorinated carboxylic acids or derivatives thereof, preferably perfluorooctanoate in acid or salified form.
- (Currently Amended) A <u>The</u> process according to claim 1, wherein the contact between the gaseous stream and the aqueous solutions is carried out in a scrubber.
- 4. (Currently Amended) A <u>The</u> process according to claim 3, wherein the <del>used</del> absorption column <u>scrubber</u> is a filling up column, preferably structured, a plate column or a spray column; preferably a spray column is used.
- (Currently Amended) A <u>The</u> process according to claim 1, wherein one the process operates in a discontinuous or a continuous way, preferably in a continuous way.

- 6. (Currently Amended) A <u>The process according to claim 5</u>, wherein one <u>the process</u> operates in <u>the [[a]] continuous way according to one of the following methods a method selected from the group consisting of:</u>
  - by recycling the solution and recovering the surfactant at each recycle[[,]];
  - by recycling the solution until reaching a surfactant concentration of 70 ppm and then by treating <u>a</u> [[the]] liquid phase to remove the surfactant[[,]];
  - by using in the gas absorption phase scrubber fresh solution without recycle[[,]]; and
  - by feeding a fresh aqueous solution aliquot and drawing from the plant scrubber an aliquot containing the anionic surfactants to be sent to a recovery plant recovered.
- 7. (Currently Amended) A <u>The</u> process according to claim 5, wherein when one <u>the</u> <u>process</u> operates in [[a]] <u>the</u> discontinuous way, the solution used in the <del>absorption</del> <u>column scrubber</u> is recycled until a surfactant concentration of 70 ppm is reached.
- 8. (Currently Amended) A <u>The</u> process according to claim 1, wherein the surfactant is recovered from the aqueous solution flowing out from the absorption column by ene of the following methods a method selected from the group consisting of:
  - by passing the solution on anionic exchange resins[[,]];
  - by using specific adsorbers for fluorinated surfactants[[,]];
  - by reverse osmosis units[[,]]; and
  - by precipitation with polivalent cation salts.
- 9. (Currently Amended) A <u>The</u> process according to claim 8, wherein a strong anionic exchange resin is used.

- 10. (Currently Amended) A <u>The process according to claim 8</u>, wherein the used specific adsorbers are selected from <u>the group consisting of active carbon</u>, aluminas, <u>and silicas</u>.
- 11. (Currently Amended) A <u>The</u> process according to claim 1, wherein the initial removal solution, and/or the recycle solution have a temperature in the range 5°C-40°C preferably 10°C-30°C.
- 12. (Currently Amended) A <u>The</u> process according to claim 1, wherein, in the scrubber, the ratio by weight among the flow rates of the feeding aqueous solution and fed <u>feed</u> gas is from 2 to 20, preferably from 4 to 15.
- 13. (New) The process of claim 1, wherein the aqueous solution density is lower than 1.03 g/cm<sup>3</sup>.
- 14. (New) The process of claim 1, wherein the concentration in the aqueous solution of the fluorinated anionic surfactant removed from the gaseous stream is lower than or equal to 60 ppm.
- 15. (New) The process of claim 1, wherein the concentration in the aqueous solution of the fluorinated anionic surfactant removed from the gaseous stream is lower than 50 ppm.
- 16. (New) The process of claim 2, wherein the anionic fluorinated surfactants are perfluorooctanoate in acid or salified form.
- 17. (New) The process of claim 4, wherein the scrubber is one member selected from the group consisting of a structured column, a plate column and a spray column.
- 18. (New) The process of claim 4, wherein the scrubber is the structured column.

- 19. (New) The process of claim 11, wherein the temperature is in the range of 10°C-30°C.
- 20. (New) The process of claim 12, wherein the ratio is from 4 to 15.